

EXPANDABLE BEADS OF STYRENE-MODIFIED LINEAR  
LOW-DENSITY POLYETHYLENE-BASED RESIN, PRODUCTION  
5       METHOD THEREFOR, PRE-EXPANDED BEADS AND  
          EXPANDED MOLDED ARTICLE

Technical Field

10       The present invention relates to expandable particles  
of a styrene-modified linear low-density polyethylene-based  
resin, production method therefor, pre-expanded particles and  
expanded molded article.

Background Art

15       A polyethylene-based resin foam is generally used as a  
packing material owing to its high resilience and excellent oil  
and impact resistance. The polyethylene-based resin foam,  
however, has drawbacks that its stiffness and compressive  
strength are low. On the other hand, a polystyrene-based  
20      resin foam is excellent in stiffness, but has a drawback that it  
is brittle.

          To overcome such drawbacks, Japanese Examined  
Patent Publication No. SHO 51(1976)-46138 and Japanese  
Unexamined Patent Publication No. SHO 62(1987)-59642  
25      disclose a method for obtaining expandable particles of a

styrene-modified polyethylene-based resin by impregnating a styrene monomer into a polyethylene-based resin for polymerization.

Examples of the polyethylene-based resin used in the  
5 method substantially include low-density polyethylene,  
high-density polyethylene, and an ethylene-vinyl acetate  
copolymer. In most cases, polyethylene is cross-linked to  
improve its moldability and physical properties of a molded  
product. The cross-linking of polyethylene increases the  
10 strength of foam membrane and also increases the tension of  
the membrane at expansion molding, so that the membrane is  
prevented from breaking and an expansion ratio can be  
increased.

Consequently, an expanded molded article with a fine  
15 appearance is provided and the impact strength of the  
expanded molded article can be increased. This method,  
however, requires that pre-crosslinked polyethylene be used or  
a cross-linking step be provided for cross-linking polyethylene  
after a temperature is furthermore raised at the end of the  
20 polymerization of styrene monomer.

To solve the above-mentioned problems, Japanese  
Patent No. 2668384 also discloses a method for obtaining an  
expanded molded article of a modified polyethylene-based resin  
excellent in stiffness and impact resistance. In this method,  
25 100 parts by weight of non-crosslinked linear low-density

polyethylene-based resin particles, 5 to 300 parts by weight of a vinyl aromatic monomer, and 1 to 3 parts by weight of a polymerization initiator relative to 100 parts by weight of the vinyl aromatic monomer are dispersed in an aqueous medium.

- 5 Then, a suspension thus obtained is heated at such a temperature that polymerization of the monomer does not substantially take place for impregnation of the monomer into an inside and a surface of the polyethylene-based resin particles. Subsequently, the temperature of the suspension is
- 10 raised to polymerize the monomer, as a result, the expanded molded article of the modified polyethylene-based resin is obtained by micro-dispersion of a vinyl aromatic polymer in polyethylene.

In Examples of the above-mentioned patent, a styrene monomer is added to linear low-density polyethylene-based resin particles having a melting point of 122 °C for polymerization at 115 °C (the melting point of the resin particles is not specified in Examples, but the present inventors confirmed from the product name of the resin particles described in Examples that the particles have the above-mentioned melting point). The polymerization at this temperature often results in graft polymerization of styrene monomer on a polyethylene chain. Consequently, though a resultant resin is not cross-linked, the graft polymerization of polystyrene on the polyethylene chain occurs, and thereby a

fine expanded molded article can be provided. Hereinafter, the term "graft polymer" means a gel component containing polystyrene, and the term "crosslinked polymer" means a gel component substantially not containing polystyrene.

5           In the above-mentioned patent, an amount of the styrene monomer is 5 to 300 parts by weight relative to 100 parts by weight of polyethylene, and when more than 300 parts by weight of the styrene monomer is impregnated into polyethylene, there is a problem that a large amount of 10 polymer powder of polystyrene is generated.

Where a styrene monomer is impregnated into polyethylene-based resin particles for polymerization to obtain a resin which is subsequently impregnated with a volatile blowing agent and molded by heating to obtain an expanded 15 molded article, polyethylene needs to be cross-linked for enhancing impact resistance of the expanded molded article and for reducing a size variation of the expanded molded article after heating. In other words, the cross-linking of polyethylene is required for the expanded molded article to 20 have heat resistance and higher stiffness. However, there has been a problem that the cross-linking involves an increase in cost due to the use of a crosslinker and an increase in a production step.

Accordingly, there has been desired development of 25 expandable particles of a styrene-modified linear low-density

polyethylene-based resin capable of providing an expanded molded article having sufficient strength, in which a ratio of styrene monomer to polyethylene can be widely changed.

5 Disclosure of Invention

The object of the present invention is to provide an expanded molded article having an improved stiffness and an excellent dimensional stability at heating while maintaining a fundamental property, i.e., excellent impact resistance that 10 polyethylene possesses, without cross-linking a polyethylene chain.

The present inventors made an extensive study to achieve the above-mentioned object and found that expandable particles of a styrene-modified linear low-density 15 polyethylene-based resin are obtained by selecting a linear low-density polyethylene-based resin as polyethylene, and by controlling selection of types and amount of a polymerization initiator and a polymerization temperature when impregnating a styrene-based monomer into the resin for polymerization. 20 The expandable particles thus obtained can control an amount of a gel component derived from, for example, graft polymerization of styrene on the polyethylene chain, and provide an expanded molded article which satisfies physical properties such as impact resistance, stiffness and heat 25 resistance. Thus, the present inventors achieved the present

invention.

According to the present invention, there is provided a method for producing expandable particles of a styrene-modified linear low-density polyethylene-based resin 5 comprising, in the order recited, the steps of:

dispersing 100 parts by weight of non-crosslinked linear low-density polyethylene-based resin particles, 30 to 300 parts by weight of a styrene-based monomer, and 0.1 to 0.9 parts by weight of a polymerization initiator relative to 100 10 parts by weight of the styrene-based monomer into a suspension containing a dispersant;

impregnating the styrene-based monomer into the low-density polyethylene-based resin particles by heating a resultant dispersion at such a temperature that polymerization 15 of the styrene-based monomer does not substantially take place;

performing a first polymerization of the styrene-based monomer at a temperature of higher than  $(T-8)$  °C and lower than  $(T+1)$  °C (where  $T$  °C is a melting point of the low-density 20 polyethylene-based resin particles);

adding a styrene-based monomer and 0.1 to 0.9 parts by weight of a polymerization initiator relative to 100 parts by weight of the styrene-based monomer when a conversion ratio of polymerization reaches to 80 to 99.9%, and performing 25 impregnation of the styrene-based monomer into the

polyethylene-based resin particles and a second polymerization of the styrene-based monomer at a temperature of higher than (T-15) °C and lower than (T+5) °C (where T °C is a melting point of the polyethylene-based resin particles) (wherein a total 5 amount of the styrene monomers used in the first and second polymerizations is more than 300 parts by weight and not more than 1000 parts by weight relative to 100 parts by weight of the low-density polyethylene-based resin particles); and  
10 impregnating a volatile blowing agent during or after the polymerization,  
whereby resin components of the expandable particles contain a gel component comprising 2 to 40 wt% of a graft polymer.  
Further, the present invention provides expandable  
15 particles of a styrene-modified linear low-density polyethylene-based resin comprising a volatile blowing agent and a base resin, the base resin containing more than 300 parts by weight and not more than 1000 parts by weight of a polystyrene-based resin component relative to 100 parts by  
20 weight of a non-crosslinked linear low-density polyethylene-based resin component, wherein the base resin contains 2 to 40 wt% of a gel component comprising a graft polymer of the low-density polyethylene-based resin component and the polystyrene-based resin component.  
25 Still further, the present invention provides

pre-expanded particles having a bulk density of 20 to 200 kg/m<sup>3</sup> obtained by pre-expanding the above-mentioned expandable particles of the styrene-modified linear low-density polyethylene-based resin.

5 Still yet, the present invention provides an expanded molded article having a density of 20 to 200 kg/m<sup>3</sup> thus obtained by expansion molding of the above-mentioned pre-expanded particles.

10 Best Mode for Carrying Out the Invention

Expandable particles of a styrene-modified linear low-density polyethylene-based resin (hereinafter referred to as expandable resin particles) obtained by the production method of the present invention comprise a volatile blowing agent and 15 a base resin containing a non-crosslinked linear low-density polyethylene-based resin component and the polystyrene-based resin component.

As the non-crosslinked linear low-density polyethylene-based resin component (hereinafter referred 20 simply to as a polyethylene-based resin component) used in the present invention, a copolymer of ethylene and an  $\alpha$ -olefin can be mentioned.

Examples of the  $\alpha$ -olefin include 1-butene, 1-pentene, 1-hexene, 3,3-dimethyl-1-butene, 4-methyl-1-pentene, 25 4,4-dimethyl-1-pentene, and 1-octene. Among those,

1-butene and 1-hexene are preferable.

A ratio of ethylene to the  $\alpha$ -olefin may vary depending upon physical properties desired and preferably in a range of 1:0.01 to 1:0.1 (weight ratio). The term "low-density" means a  
5 density in a range of 0.910 to 0.925 g/ml.

Low-density polyethylene, high-density polyethylene, an ethylene-propylene copolymer, an ethylene-vinyl acetate copolymer and an ethylene-acrylic acid copolymer which have a cross-link and/or a branched chain, and two or more types  
10 of these polymers may be used to such an extent that a desirable effect of the invention is not suppressed.

Examples of the polystyrene-based resin component include resin components derived from monomers such as styrene,  $\alpha$ -methylstyrene, vinyltoluene, and chlorostyrene.

15 An amount of the polystyrene-based resin component is more than 300 parts by weight and not more than 1000 parts by weight, and preferably more than 300 parts by weight and not more than 900 parts by weight relative to 100 parts by weight of the polyethylene-based resin component.

20 While it is difficult to obtain the expandable resin particles uniformly containing not less than 300 parts by weight of the polystyrene resin component by conventional methods, the present invention can easily obtain the particles in a proper manner. In the case where the amount of  
25 polystyrene-based resin component exceeds 1000 parts by

weight, characteristics of the polyethylene-based resin component, i.e., high resilience and excellent oil and impact resistance are hardly displayed. Furthermore, since styrene is not sufficiently absorbed into an inside of the

5      polyethylene-based resin component and is polymerized alone, a large amount of polymer powder is generated.

As the volatile blowing agent, for example, a hydrocarbon such as propane, butane, isobutene, pentane, isopentane, cyclopentane, and hexane may be used alone, or

10     two or more types of these hydrocarbons may be used in combination.

A content of the blowing agent is preferably 5 to 10 parts by weight relative to 100 parts by weight of the resin component (an amount of the polyethylene-based resin

15     component and the polystyrene-based resin component in total) which constitute the expandable resin particles.

In the present invention, 2 to 40 wt% of the gel component (gel fraction) comprising the graft polymer of the polyethylene-based resin component and the polystyrene-based

20     resin component is contained in the base resin of the expandable resin particles. A criterion for judging whether or not the gel component is a graft polymer is the presence or absence of polystyrene in the gel component. In the present invention, the gel component containing 10 wt% or more of

25     polystyrene is defined as the graft polymer. A method for

determining a polystyrene content in the gel component is described in Examples.

A gel fraction of less than 2 wt% is not preferable since changes in dimension of the expanded molded article at 5 heating and the impact resistance are not sufficiently improved. On the other hand, the gel fraction of more than 40 wt% is also not preferable since the strength of cell membranes is too high and elongation at formation of the expanded molded article is poor, resulting in deterioration of the expanded molded article 10 in appearance. Thus, the gel fraction is preferably 5 to 35 wt%.

Preferably, the expandable resin particles each have a substantially spherical shape or a cylindrical shape having an L/D (where L is a length of each particle and D is a diameter of 15 each particle) of 0.6 to 1.6, and an average particle size of 0.3 to 2.0 mm.

The particles having a high ovality such that the L/D is not more than 0.6 and not less than 1.6 are not preferable since the expandable resin particles have poor mold fillability 20 when they are pre-expanded as expandable styrene-modified resin particles and filled into a mold to obtain the expanded molded article. The shape of the expandable resin particles preferably is substantially spherical to improve the mold fillability.

25 The average particle size of less than 0.3 mm is not

preferable because a retention of the blowing agent decreases and a reduction of density of the expanded molded article is difficult. The average particle size of more than 2.0 mm is also not preferable since not only the particles have poor mold 5 fillability, but also thinning of the expanded molded article is difficult.

A production method for the expandable resin particles of the invention will hereinafter be described.

Where the amount of styrene-based monomer exceeds 10 300 parts by weight relative to 100 parts by weight of the polyethylene-based resin particles, the amount of polymer powder of polystyrene tends to increase when only a single impregnation is performed. To minimize the generation of the polymer powder, the styrene-based monomers are impregnated 15 into the polyethylene-based resin particles in two separate steps as described below.

Preferably, the polyethylene-based resin particles used in the method each have the substantially spherical shape or the cylindrical shape having an L/D (where L is a length of 20 each particle and D is a diameter of each particle) of 0.6 to 1.6, and preferably have an average particle size of 0.2 to 1.5 mm. The polyethylene-based resin particles having a high ovality such that the L/D is not more than 0.6 and not less than 1.6 are not preferable since the polyethylene-based resin particles 25 have poor mold fillability when they are pre-expanded as the

expandable styrene-modified resin particles and filled into a mold to obtain the expanded molded article. The shape of the polyethylene-based resin particles preferably is substantially spherical to improve mold fillability. The average particle size 5 of less than 0.2 mm is not preferable since a retention of the blowing agent decreases and a reduction of the density of the expanded molded article is difficult. The average particle size of more than 1.5 mm is also not preferable because not only the particles have poor mold fillability, but also thinning of the 10 expanded molded article is difficult.

Examples of an aqueous medium which is a component of the suspension include water and a mixed medium of water and an aqueous solvent (e.g., a lower alcohol).

15 A dispersant is not particularly limited and any conventional dispersant may be used. Specifically, the dispersant may be practically insoluble inorganic substances such as calcium phosphate, magnesium pyrophosphate, sodium pyrophosphate, and magnesium oxide.

20 A polymerization initiator may be one that is generally used as a suspension polymerization initiator of the styrene-based monomer. However, a gel generation rate varies depending upon a type of the polymerization initiator to be used. For example, use of t-butyl peroxybenzoate, dicumyl 25 peroxide, t-butyl-peroxy-2-ethylhexyl carbonate,

2, 5-dimethyl-2, 5-di-t-butylperoxyhexane or the like which abstracts more hydrogen atoms increases the amount of gel to be generated. On the other hand, use of t-butyl peroxy-3, 5, 5-trimethylhexanoate, t-butyl peroxyacetate, 2, 2-di-t-butyl 5 peroxybutane or the like which abstracts less hydrogen atoms decreases the amount of gel to be generated. The above-mentioned polymerization initiators may be adopted alone, or two or more types of these polymerization initiators may be used in combination depending upon a desirable gel 10 fraction.

An amount of the polymerization initiator is preferably 0.1 to 0.9 parts by weight, and more preferably 0.2 to 0.5 parts by weight relative to 100 parts by weight of the styrene-based monomer. The polymerization initiator in an amount of less 15 than 0.1 parts by weight is not preferable since styrene is not smoothly polymerized, and thereby polystyrene and polyethylene are not homogeneously mixed in the resin particles and a larger amount of polymer powder is generated. Use of the polymerization initiator in an amount of more than 20 0.9 parts by weight decreases a molecular weight of the polystyrene-based resin.

A molecular weight of polystyrene-based resin component is preferably about 200,000 to 400,000 to achieve fine physical properties. The polymerization initiator in an 25 amount of more than 0.9 parts by weight can only achieve a

styrene molecular weight less than the above range.

An amount of the styrene-based monomer used in the first polymerization is in a range of 30 to 300 parts by weight relative to 100 parts by weight of the polyethylene-based resin particles. The styrene-based monomer in an amount of less than 30 parts by weight is not preferable since the styrene-based monomer is not homogeneously impregnated into polyethylene. The styrene-based monomer in an amount of more than 300 parts by weight is not preferable since the polymer powder derived from the styrene-based monomer is more easily generated.

The resultant dispersion is heated to such a temperature that polymerization of the styrene-based monomer does not substantially take place to impregnate the styrene-based monomer into the polyethylene-based resin particles.

An appropriate time required for impregnating the styrene-based monomer into the inside of the polyethylene-based resin particles is 30 minutes to 2 hours, since when the polymerization proceeds before the styrene-based monomer is sufficiently impregnated into the resin particles, the polymer powder of polystyrene is generated. The temperature at which the styrene-based monomer is substantially not polymerized should be higher to accelerate an impregnation rate, but the temperature needs to be determined

in due consideration of a decomposition temperature of the polymerization initiator.

The first polymerization of the styrene-based monomer is carried out at a temperature of (T-8) to (T+1) °C (where T °C 5 is the melting point of the above-mentioned polyethylene-based resin particles). Where the polymerization temperature is lower than (T-8) °C or higher than (T+1) °C, sufficient graft polymerization can not be achieved.

When the conversion ratio of polymerization reaches 10 to 80 to 99.9%, the styrene-based monomer and 0.1 to 0.9 parts by weight of the polymerization initiator relative to 100 parts by weight of the styrene-based monomer are added, and the temperature is set to (T-15) to (T+5) °C (where T °C is the melting point of the polyethylene-based resin particles), so that 15 the impregnation of the styrene-based monomer into the low-density polyethylene-based resin particles and a second polymerization are performed. The amount of the styrene-based monomer used in the first and second polymerization in total is more than 300 parts by weight and 20 not more than 1000 parts by weight.

Where more than 300 parts by weight of the styrene-based monomer is added when the conversion ratio of polymerization reaches to 80%, the styrene-based monomer is quickly impregnated into the polyethylene-based resin particles 25 for quick polymerization, whereby the generation of polymer

powder of polystyrene can be suppressed. When the conversion ratio of polymerization exceeds 99.9%, the impregnation of the styrene-based monomer added is difficult and a conversion ratio decreases, causing the generation of the 5 powdered particles difficult to be suppressed.

A mixed solution containing the styrene-based monomer and the polymerization initiator may be added continuously or intermittently for the second polymerization. To prevent the generation of the polymer powder, the 10 impregnation into the inside of the polyethylene-based resin particles and the polymerization are preferably performed at almost the same time. A fast addition rate is not preferable because the fast addition rate in combination with a relatively high polymerization temperature causes the polymerization to 15 occur before the resin particles are impregnated. An extremely slow addition rate is not preferable since it may hinder the polymerization. For example, the addition rate for 300 to 1000 parts by weight of the styrene-based monomer is 3 to 5 hours.

20 Furthermore, the polymerization temperature of the second polymerization preferably ranges from (T-8) to (T+1) °C, so that the graft polymerization occurs more efficiently.

The volatile blowing agent is impregnated into the resin particles during or after the polymerization, so that the 25 expandable resin particles are obtained. This impregnation of

the blowing agent can be performed by a per se known method.

For example, the impregnation during polymerization can be carried out by conducting the polymerization in a closed vessel, and by injecting the volatile blowing agent into the vessel.

- 5     The impregnation after the polymerization is carried out by injecting the volatile blowing agent into a closed vessel. In the impregnation after the polymerization, a vessel for the polymerization may not be a closed vessel as long as the impregnation is carried out in the closed vessel.

10                 The expandable resin particles of the present invention thus obtained may serve as pre-expanded particles by pre-expanding the expandable resin particles to a predetermined bulk density (e.g., 20 to 200 kg/m<sup>3</sup>) by a conventional method. A method for determining the bulk density will be described in Examples.

15                 Furthermore, an expanded molded article is provided by filling the pre-expanded particles into a mold and heating the pre-expanded particles again to allow them to fuse together by heat while expansion.

20                 As a medium for heating the pre-expanded particles, steams are suitably used. A density of the expanded molded article is preferably 20 to 200 kg/m<sup>3</sup>. The expanded molded article having a density of less than 20 kg/m<sup>3</sup> is not preferable since sufficient strength is not achieved. The expanded  
25                 molded article having a density of more than 200 kg/m<sup>3</sup> is also

not preferable since a reduction in weight can not be achieved and the expanded molded article may not be able to sufficiently exert characteristics of polyethylene including resilience.

The expanded molded article thus obtained is tough  
5 and excellent in impact strength. Furthermore, the expanded  
molded article has high stiffness due to the modification of  
styrene.

A falling ball impact value of the expanded molded  
article is preferably 85 cm or more. The expanded molded  
10 article having a falling ball impact value of less than 85 cm  
may be used, but if the expanded molded article has a falling  
ball impact value of not less than 85 cm, it is applicable to  
packing materials, etc. for fragile products and heavy  
components. The falling ball impact value of the expanded  
15 molded article is more preferably 90 cm or more. A method  
for measuring the falling ball impact value will be described in  
Examples.

The expanded molded article of the present invention  
may be used for various purposes, and particularly suitable for  
20 material for interior furnishings of a car, energy absorbing  
material to be inserted inside a bumper, packing material for  
heavy products, and the like.

#### Examples

25 The present invention will hereunder be described

with reference to Examples and Comparative Examples, but it should be understood that the invention be not limited by these Examples and Comparative Examples. Methods for determining values shown in Examples and Comparative

5 Examples are described below.

(Determination of gel fraction)

For determination of a gel fraction, a sample of resin particles was weighed, the sample was put in a flask, and 100 ml of toluene was added. The particles were then dissolved in 10 an oil bath at 130 °C for 24 hours. After the flask was taken out from the oil bath, a resultant mixture was immediately filtered by an 80-mesh ( $\phi$  0.12 mm) wire gauze, and a sample remaining on the wire gauze which is insoluble in boiling toluene and the wire gauze were then allowed to stand in an 15 oven at 130 °C for an hour to remove toluene, and a weight of the resultant solid was measured. The gel fraction is determined by the following equation:

$$\frac{\text{Weight of resultant solid}}{\text{Weight of sample}} \times 100 = \text{gel fraction (wt\%)}$$

20 About 200  $\mu$  g of the resultant solid was weighed and enwrapped in a ferromagnetic metal (Pyrofoil: manufactured by Japan Analytical Industry Co., Ltd.) so as to be in close contact with each other. Then, a pyrolysate was generated using a pyrolysis apparatus called Curie Point Pyrolyzer Model

JHP-3 (manufactured by Japan Analytical Industry Co., Ltd.).  
The pyrolysate was analyzed using Gas Chromatograph Auto  
System (manufactured by Perkin Elmer) to determine an  
polystyrene content from the analytical result. The following  
5 analytical conditions were adopted. Pyrolysis temperature:  
590 °C-5 sets, oven temperature: 280 °C, needle temperature:  
300 °C, column: DB-5 (0.25 μ m × φ 0.25 mm × 30 m,  
manufactured by J & W), column temperature: 50 °C(1 min)→  
temperature rise of 10 °C/min→100 °C→temperature rise of  
10 40 °C/min→320 °C(3.5 min), carrier gas: He, carrier flow rate:  
1 ml/min, pressure at column inlet: 12 psi, temperature at  
column inlet: 300 °C, temperature of a detector: 300 °C, and  
detector: FID. Determination was made by an absolute  
calibration curve method using polystyrene resin QC254  
15 manufactured by Asahi Kasei Co., as a standard sample.

When the polystyrene content is 10 wt% or more, it  
was determined that a gel component comprises a graft  
polymer but not a cross-linked polymer.

(Measurement of powder content)

20 For measurement of a powder content, about 1000 g of  
a polymerized slurry sample was introduced into a polymer  
beaker having a water vent with 35-mesh wire gauze attached  
on its top. Into this beaker about 6 liter of wash water was  
gradually introduced, and liquid flowed out of the vent was  
25 collected. The collected liquid was filtered by a glass fiber

paper filter (GA-100) and dried in an oven at 60 °C for 3 hours to measure the weight of dried polymer powder. The resin remained in the slurry sample after washing was dried and weighed as well. The powder content was determined by the  
5 following equation:

$$\frac{\text{Weight of powder resin (g)}}{\text{Weight of dried resin (g)}} \times 100 = \text{powder content (wt\%)}$$

(Measurement of molecular weight of polystyrene resin component in resin particles)

10 An average molecular weight (Mw) of a polymer was measured by GPC (Gel Permeation Chromatography) under the following conditions.

Measuring equipment:

15 High-speed GPC equipment HLC-8020 manufactured by Tosoh Corp.  
Column: HSG-60S × 2, HSG-40H × 1, HSG-20H × 1  
manufactured by Sekisui Fine Chemicals Co., Ltd.

Measuring conditions:

20 Column temperature: 40 °C  
Moving bed: THF (tetrahydrofuran)  
Flow rate: 1.0 ml/min  
Injection amount: 500 ml  
Detector: RID-6A

manufactured by Tosoh Corp.

Molecular weight determination of the sample:

For measuring a molecular weight of a sample, conditions for measuring were selected so that a molecular weight

5 distribution of the sample overlaps a range of a linear calibration curve correlating a count number with a logarithm of the molecular weight of various monodisperse polystyrene standard samples.

In the present invention, the calibration curve for  
10 polystyrene was plotted using six polystyrene standard samples (TSK standard polystyrene) respectively having a weight-average molecular weight of  $2.74 \times 10^3$ ,  $1.91 \times 10^4$ ,  $1.02 \times 10^5$ ,  $3.55 \times 10^5$ ,  $2.89 \times 10^6$ ,  $4.48 \times 10^6$  manufactured by Tosoh Corp.

15 (Determination of bulk density)

A bulk density was determined according to a method described in JIS K 6911:1955 "General Testing Methods for Thermosetting Plastics". Specifically, pre-expanded particles free-falling into a graduated cylinder by an apparent density  
20 measuring instrument was weighed to determine their bulk density by the following equation.

bulk density ( $\text{kg}/\text{m}^3$ ) = weight ( $\text{kg}$ )/particle volume in the graduated cylinder ( $\text{m}^3$ )

(Determination of density of expanded molded article)

25 A density of an expanded molded article was

determined according to a method described in JIS A 9511:1995 "Preformed Cellular Plastics Thermal Insulation Materials".

(Measurement of compressive strength)

5       A compressive strength was measured according to a method described in JIS A 9511:1995 "Preformed Cellular Plastics Thermal Insulation Materials". In other words, the compressive strength of a test specimen having a size of 50×50×50 mm was measured when it was compressed by 5%  
10      using a universal testing machine Tensilon UCT-10T (manufactured by Orientech Co.) under a compressive rate of 10 mm/min.

(Measurement of impact strength)

For measurement of impact strength, an expanded  
15      molded article was cut to form a sample having a size of 215×40×20 mm, and the sample was then placed on a pair of holding members arranged at a distance of 155 mm. A steel ball weighing 321 g was added on the middle of the sample in width direction thereof at a position halfway between the pair  
20      of holding members to see whether or not the sample was crushed.

The test was repeated at different heights of drop and the minimum height of drop that produced crush on the sample was defined as a falling ball impact value to evaluate  
25      the impact strength. Thus, the impact strength increases as

the falling ball impact value increases.

(Determination of dimensional change rate under heat)

A flat-shaped expanded molded article having a size of 400 mm length, 300 mm width, and 16 mm thickness was  
5 taken out from a mold, and allowed to stand at a constant temperature for 24 hours in a thermohygrostat (in a state of standard temperature of 23 °C and 50% relative humidity of JIS-K7100). Then, a flat square board (150 mm length, 150 mm width, and 16 mm thickness) having parallel, upper and  
10 lower surfaces was cut out from the center of the expanded molded article. On the middle of the board, three straight parallel lines were drawn respectively in vertical and lateral direction so as to be 50 mm apart from each other to form a specimen that complies with JIS-K6767. After the specimen  
15 was measured for its dimension (dimension before heating: L1), it was placed horizontally in an oven with internal air circulation maintained at 80 °C. The specimen was then taken out from the oven after being heated for 168 hours, and again allowed to stand at the constant temperature for an hour  
20 in the thermohygrostat to measure the specimen for its dimension (dimension after heating: L2). The measurement of dimensions before and after the heating test was carried out in compliance with JIS-K6767, and a dimensional change rate was determined by the following equation.  
25 dimensional change rate (%) =  $(L2-L1) \times 100/L1$

(wherein L1 is a dimension of the specimen obtained from the expanded molded article after it was molded and kept standing at 23°C and 50% RH for 24 hours. L2 is a dimension of the specimen after the expanded molded article was heated at 5 80 °C for 168 hours.)

The dimension of the specimen is an average length of the three lines provided both in vertical and horizontal directions of the specimen obtained from the expanded molded article.

10 It was determined that the expanded molded article with a dimensional change rate of 0.5% or less has heat resistance.

Example 1

(Production of polyethylene-based resin particles)

15 Linear low-density polyethylene (ethylene-hexene copolymer, melt index of 1.0 g/10 min, density of 0.921 g/ml, melting point of 126 °C) was granulated by an extruder to obtain polyethylene-based resin particles of substantially spherical shape having an L/D of 0.9 and an average particle 20 size of 0.8 mm. As a foam regulator, 0.5 parts by weight of talc relative to 100 parts by weight of the above-mentioned polyethylene was added at the granulation.

(Production of styrene-modified polyethylene-based resin particles)

25 40 kg of pure water, 200 g of magnesium

pyrophosphate as a dispersant, and 20 g of sodium dodecylbenzenesulfonate were introduced in an autoclave having an internal volume of 100 liter to prepare an aqueous medium. 8 kg of the above-mentioned polyethylene-based resin particles was suspended in the aqueous medium and stirred at 150 rpm.

10        Into the autoclave, a mixed solution containing 16 kg of a styrene monomer (200 parts by weight relative to 100 parts by weight of polyethylene) and 48 g of t-butylperoxy-2-ethylhexylcarbonate (TBPOEHC) (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) as a polymerization initiator was added and allowed to stand at 60 °C for 60 minutes to impregnate the styrene monomer into the polyethylene-based resin.

15        Then, the temperature was raised to 119 °C and polymerization was carried out for 3 hours. After a conversion ratio of polymerization of the styrene monomer reached to 85%, a mixed solution containing 16 kg of the styrene monomer (200 parts by weight relative to 100 parts by weight of polyethylene) and 48 g of t-butylperoxybenzoate (TBPB) (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) as a polymerization initiator was added over a period of 3 hours to perform polymerization while impregnating the styrene monomer into the inside of polyethylene. Then, by raising to 140 °C and maintained for

2 hours, the remaining monomer was forcibly polymerized to reduce its amount, and then the autoclave was cooled to take out styrene-modified polyethylene-based resin particles.

The gel fraction measured was 7.2 wt%. The  
5 polystyrene content in the gel component was 22.2 wt% and the powder content in the polymerized slurry was 0.7 wt%. The molecular weight of the polystyrene resin component was about 320,000.

(Production of expandable particles of  
10 styrene-modified polyethylene-based resin and evaluations of their expandability and moldability)

20 kg of the above-mentioned styrene-modified polyethylene-based resin particles and 400 g of toluene were introduced into a pressure-resistant twin-cylinder mixer which  
15 has an internal volume of 50 liter and can be hermetically sealed. After the mixer was hermetically sealed, it was rotated and 2800 g of butane (n-butane: i-butane = 7: 3, volume ratio, butane with the same volume ratio was used in the following Examples) was forced into the mixer. Then, the  
20 temperature was raised to 70 °C and maintained for 4 hours to impregnate butane into the particles. The mixer was then cooled and expandable particles of a styrene-modified polyethylene-based resin were taken out.

The expandable resin particles taken out from the  
25 mixer were immediately pre-expanded by steam to have a bulk

density of 33 kg/m<sup>3</sup>. About 24 hours later, the pre-expanded resin particles were filled into a mold and heated by steam to allow them to fuse together while being pre-expanded, so that an expanded molded article having a density of 33 kg/m<sup>3</sup> are 5 obtained. The expanded molded article thus obtained had excellent strength, showing a compressive strength of 40 N/cm<sup>2</sup> and falling ball impact value as high as 85 cm. The dimensional change rate was 0.4%.

Example 2

10 The same polymerization procedure as in Example 1 was repeated except that the temperature for polymerization was 121 °C, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

15 The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The gel fraction measured was 26.5 wt%. The polystyrene content in the gel component was 31.9 wt%, and the powder content in the polymerized slurry was 0.8 wt%. The molecular weight of the polystyrene resin component was 20 about 310,000.

The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 42 N/cm<sup>2</sup>, and falling ball impact value as high as 95 cm. The dimensional change rate under heat was 0.3%.

Example 3

The same polymerization procedure as in Example 1 was repeated except that the temperature for polymerization was 122 °C, to obtain styrene-modified polyethylene-based 5 resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction measured was 33.5 wt%. The polystyrene content in the gel component was 20.9 wt% and the powder content in the polymerized slurry was 0.7 wt%.  
10 The molecular weight of the polystyrene resin component was about 300,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive 15 strength of 44 N/cm<sup>2</sup>, and falling ball impact value as high as 95 cm. The dimensional change rate under heat was 0.2%.

Example 4

The same polymerization procedure as in Example 1 was repeated except that the temperature for polymerization 20 was 123 °C, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction measured was 20.8 wt%. The polystyrene content in the gel component was 22.1 wt% and 25 the powder content in the polymerized slurry was 0.6 wt%.

The molecular weight of the polystyrene resin component was about 290,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had 5 excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 42 N/cm<sup>2</sup>, and falling ball impact value as high as 90 cm. The dimensional change rate under heat was 0.3%.

#### Example 5

The same polymerization procedure as in Example 1 10 was repeated except that the temperature for polymerization was 125 °C, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction measured was 5.8 wt%. The 15 polystyrene content in the gel component was 34.5 wt% and the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 280,000.

The pre-expanded resin particles had a bulk density of 20 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 40 N/cm<sup>2</sup>, and falling ball impact value as high as 85 cm. The dimensional change rate under heat was 0.4%.

#### Example 6

25 40 kg of pure water, 200 g of magnesium

pyrophosphate as a dispersant, and 20 g of sodium dodecylbenzenesulfonate were introduced in an autoclave having an internal volume of 100 liter to prepare an aqueous medium. 4.4 kg of the polyethylene-based resin particles 5 obtained in Example 1 was suspended in the medium and stirred at 150 rpm.

Into the autoclave, a mixed solution containing 13.2 kg of a styrene monomer (300 parts by weight relative to 100 parts by weight of polyethylene) and 39.6 g of TBPOEHC (0.3 10 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60 minutes to impregnate the styrene monomer into the polyethylene-based resin.

Then, the temperature was raised to 122 °C and 15 polymerization was carried out for 3 hours. After the conversion ratio of polymerization of the styrene monomer reached to 85%, a mixed solution containing 22.4 kg of a styrene monomer (500 parts by weight relative to 100 parts by weight of polyethylene) and 67.2 g of TBPB (0.3 parts by weight 20 relative to 100 parts by weight of the styrene monomer) was added at 122 °C over a period of 5 hours to perform polymerization while impregnating the styrene monomer into the inside of polyethylene. Then, by raising to 140 °C and maintained for 2 hours, the remaining monomer was forcibly 25 polymerized to reduce its amount, and then the autoclave was

cooled to take out styrene-modified polyethylene-based resin particles.

The gel fraction measured was 38.5 wt%. The polystyrene content in the gel component was 21.3 wt% and 5 the powder content in the polymerized slurry was 0.8 wt%. The molecular weight of the polystyrene resin component was about 300,000.

The same procedure as in Example 1 was repeated except that the obtained resin particles were used, so that a 10 pre-expanded resin particles having a bulk density of 33 kg/m<sup>3</sup> and an expanded molded article having a density of 33 kg/m<sup>3</sup> were obtained. The expanded molded article thus obtained had excellent strength, showing a compressive strength of 48 N/cm<sup>2</sup> and falling ball impact value as high as 85 cm. The 15 dimensional change rate under heat was 0.2%.

#### Example 7

40 kg of pure water, 200 g of magnesium pyrophosphate as a dispersant, and 20 g of sodium dodecylbenzenesulfonate were introduced in an autoclave 20 having an internal volume of 100 liter to prepare an aqueous medium. 8.0 kg of the polyethylene-based resin particles obtained in Example 1 was suspended in the medium and stirred at 150 rpm.

Into the autoclave, a mixed solution containing 8.0 kg 25 of a styrene monomer (100 parts by weight relative to 100

parts by weight of polyethylene) and 24.0 g of TBPB (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60 minutes to impregnate the styrene monomer into the

5 polyethylene-based resin particles. Then, the temperature was raised to 119 °C and polymerization was carried out for 3 hours. After the conversion ratio of polymerization of the styrene monomer reached to 85%, a mixed solution containing 24.0 kg of a styrene monomer (300 parts by weight relative to

10 100 parts by weight of polyethylene), and 27.0 g of TBPB (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added at 121 °C over a period of 4 hours to perform polymerization while impregnating styrene into the inside of polyethylene. Then, by raising to 140 °C and

15 maintained for 2 hours, the remaining monomer was forcibly polymerized to reduce its amount, and then the autoclave was cooled to obtain styrene-modified polyethylene-based resin particles. Pre-expanded resin particles and an expanded molded article were subsequently obtained in the same manner

20 as in Example 1.

The gel fraction in the resin particles thus obtained was 7.2 wt%. The polystyrene content in the gel component was 25.0 wt% and the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene

25 resin component was about 300,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 43 N/cm<sup>2</sup>, and falling ball impact value as high as 5 85 cm. The dimensional change rate under heat was 0.4%.

Example 8

The same polymerization procedure as in Example 7 was repeated except that the temperature for the first polymerization was 126 °C and that DCP was used as the 10 polymerization initiator for the first polymerization, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction in the resin particles thus obtained 15 was 3.5 wt%. The polystyrene content in the gel component was 22.8 wt% and the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 300,000.

The pre-expanded resin particles had a bulk density of 20 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 42 N/cm<sup>2</sup>, and falling ball impact value as high as 85 cm. The dimensional change rate under heat was 0.4%.

Example 9

25 The same polymerization procedure as in Example 7

was repeated except that the temperatures for the first and second polymerization were 123 °C and 112 °C, respectively, and that t-butylperoxy-3, 5, 5-trimethylhexanoate (TBPOTMH) was used as the polymerization initiator for the second 5 polymerization, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction in the resin particles thus obtained was 3.2 wt%. The polystyrene content in the gel component 10 was 24.4 wt% and the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 340,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had 15 excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 43 N/cm<sup>2</sup>, and falling ball impact value as high as 85 cm. The dimensional change rate under heat was 0.3%.

#### Example 10

The same polymerization procedure as in Example 7 20 was repeated except that the temperatures for the first and second polymerization were 123 °C and 130 °C, respectively, and that DCP was used as the polymerization initiator for the first polymerization, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin 25 particles and an expanded molded article thereof.

The gel fraction in the resin particles thus obtained was 3.8 wt%. The polystyrene content in the gel component was 24.2 wt% and the powder content in the polymerized slurry was 0.6 wt%. The molecular weight of the polystyrene 5 resin component was about 240,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 43 N/cm<sup>2</sup>, and falling ball impact value as high as 10 85 cm. The dimensional change rate under heat was 0.4%.

Example 11

40 kg of pure water, 200 g of magnesium pyrophosphate as a dispersant, and 20 g of sodium dodecylbenzenesulfonate were introduced in an autoclave 15 having an internal volume of 100 liter to prepare an aqueous medium. 8.0 kg of the polyethylene-based resin particles obtained in Example 1 was suspended in the medium and stirred at 150 rpm.

Into the autoclave, a mixed solution containing 8.0 kg 20 of a styrene monomer (100 parts by weight relative to 100 parts by weight of polyethylene) and 48.0 g of TBPB (0.6 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60 minutes to impregnate the styrene monomer into the 25 polyethylene-based resin particles. Then, the temperature

was raised to 120 °C and polymerization was carried out for 3 hours.

After the conversion ratio of polymerization of the styrene monomer reached to 90%, a mixed solution containing 5 24.0 kg of a styrene monomer (300 parts by weight relative to 100 parts by weight of polyethylene) and 144.0 g of TBPB (0.6 parts by weight relative to 100 parts by weight of the styrene monomer) was added at 120 °C over a period of 4 hours to perform polymerization while impregnating styrene into the 10 inside of polyethylene. Then, by raising to 140 °C and maintained for 2 hours, the remaining monomer was forcibly polymerized to reduce its amount, and then the autoclave was cooled to obtain styrene-modified polyethylene-based resin particles. Pre-expanded resin particles and an expanded 15 molded article were subsequently obtained in the same manner as in Example 1.

The gel fraction in the resin particles thus obtained was 19.6 wt%. The polystyrene content in the gel component was 25.0 wt% and the powder content in the polymerized 20 slurry was 0.7 wt%. The molecular weight of the polystyrene resin component was about 260,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive 25 strength of 40 N/cm<sup>2</sup>, and falling ball impact value as high as

90 cm. The dimensional change rate under heat was 0.3%.

Example 12

The same polymerization procedure as in Example 11 was repeated except that the respective amount of the 5 polymerization initiators for the first and second polymerization was 0.3 parts by weight and that the mixed solution for the second polymerization was added after the conversion ratio of polymerization reached to 95%, to obtain styrene-modified polyethylene-based resin particles, 10 pre-expanded resin particles and an expanded molded article thereof.

The gel fraction measured was 18 wt%. The polystyrene content in the gel component was 23.3 wt% and the powder content in the polymerized slurry was 0.3 wt%. 15 The molecular weight of the polystyrene resin component was about 320,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive 20 strength of 46 N/cm<sup>2</sup>, and falling ball impact value as high as 95 cm. The dimensional change rate under heat was 0.2%.

Example 13

40 kg of pure water, 200 g of magnesium pyrophosphate as a dispersant, and 20 g of sodium 25 dodecylbenzenesulfonate were introduced in an autoclave

having an internal volume of 100 liter to prepare an aqueous medium. 8.0 kg of the polyethylene-based resin particles obtained in Example 1 was suspended in the medium and stirred at 150 rpm.

5            Into the autoclave, a mixed solution containing 8.0 kg of a styrene monomer (100 parts by weight relative to 100 parts by weight of polyethylene) and 19.20 g of TBPB (0.24 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60

10          minutes to impregnate the styrene monomer into the polyethylene-based resin particles. Then, the temperature was raised to 120 °C and polymerization was carried out for 3 hours. After the conversion ratio of polymerization of the styrene monomer reached to 90%, a mixed solution containing

15          24.0 kg of a styrene monomer (300 parts by weight relative to 100 parts by weight of polyethylene) and 57.6 g of TBPB (0.24 parts by weight relative to 100 parts by weight of the styrene monomer) was added at 120 °C over a period of 4 hours to perform polymerization while impregnating styrene into the

20          inside of polyethylene. Then, by raising to 140 °C and maintained for 2 hours, the remaining monomer was forcibly polymerized to reduce its amount, and then the autoclave was cooled to obtain styrene-modified polyethylene-based resin particles. Pre-expanded resin particles and an expanded

25          molded article were subsequently obtained in the same manner

as in Example 1.

The gel fraction in the resin particles thus obtained was 17.5 wt%. The polystyrene content in the gel component was 24.6 wt% and the powder content in the polymerized 5 slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 320,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a density of 33 kg/m<sup>3</sup>, a compressive strength of 46 N/cm<sup>2</sup>, and 10 falling ball impact value of 95 cm. The dimensional change rate under heat was 0.2%.

#### Comparative example 1

The same polymerization procedure as in Example 1 was repeated except that the temperature for polymerization 15 was 117 °C, and the styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof were obtained.

The gel fraction measured was 0.3 wt%. The polystyrene content in the gel component was 26.6 wt% and 20 the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 330,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a 25 density of 33 kg/m<sup>3</sup>, a compressive strength of 36 N/cm<sup>2</sup>, and

falling ball impact value of 80 cm. The dimensional change rate under heat was 0.8%.

Comparative example 2

The same polymerization procedure as in Example 1  
5 was repeated except that the temperature for polymerization was 130 °C and dicumyl peroxide (DCP) was adopted as the polymerization initiators, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

10 The gel fraction measured was 0.8 wt%. The polystyrene content in the gel component was 25.0 wt% and the powder content in the polymerized slurry was 0.8 wt%. The molecular weight of the polystyrene resin component was about 240,000.

15 The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 38 N/cm<sup>2</sup>, and falling ball impact value as high as 80 cm. However, the dimensional change rate under heat was  
20 0.7%.

Comparative example 3

The same polymerization procedure as in Example 1 was repeated except that an additional styrene monomer was added when the conversion ratio of polymerization reached to  
25 60%, to obtain styrene-modified polyethylene-based resin

particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction measured was 5.6 wt%. The polystyrene content in the gel component was 21.4 wt% and 5 the powder content in the polymerized slurry was 1.6 wt%. The molecular weight of the polystyrene resin component was about 320,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a 10 density of 33 kg/m<sup>3</sup>. Since the polymerization did not occur smoothly, a large amount of polymer powder of polystyrene was generated, whereby fusibility of expanded particles was decreased. Consequently, the compressive strength was 38 N/cm<sup>2</sup>, and falling ball impact value was 60 cm. The 15 dimensional change rate under heat was 0.8%.

#### Comparative Example 4

The same polymerization procedure as in Example 7 was repeated except that the temperatures for the first and second polymerization were 117 °C and 121 °C, respectively, to 20 obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction in the resin particles thus obtained was 1.6 wt%. The polystyrene content in the gel component 25 was 25.0 wt% and the powder content in the polymerized

slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 300,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a 5 density of 33 kg/m<sup>3</sup>, a compressive strength of 38 N/cm<sup>2</sup>, and falling ball impact value of 80 cm. The dimensional change rate under heat was 0.7%.

#### Comparative Example 5

The same polymerization procedure as in Example 7 10 was repeated except that the temperature for the first polymerization was 128 °C and that DCP was adopted as the polymerization initiator for the first polymerization, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article 15 thereof.

The gel fraction in the resin particles thus obtained was 1.8 wt%. The polystyrene content in the gel component was 25.0 wt% and the powder content in the polymerized slurry was 0.6 wt%. The molecular weight of the polystyrene 20 resin component was about 300,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a density of 33 kg/m<sup>3</sup>, a compressive strength of 40 N/cm<sup>2</sup>, and falling ball impact value of 80 cm. The dimensional change 25 rate under heat was 0.7%.

Comparative Example 6

The same polymerization procedure as in Example 7 was repeated except that the temperatures for the first and second polymerization were 123 °C and 110 °C, respectively,  
5 and that TBPOTMH was adopted as the polymerization initiator for the second polymerization, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

The gel fraction in the resin particles thus obtained  
10 was 2.6 wt%. The polystyrene content in the gel component was 25.0 wt% and the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 360,000.

The pre-expanded resin particles had a bulk density of  
15 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a density of 33 kg/m<sup>3</sup>, a compressive strength of 37 N/cm<sup>2</sup>, and falling ball impact value of 50 cm. The dimensional change rate under heat was 0.4%.

Comparative Example 7

20 The same polymerization procedure as in Example 7 was repeated except that the temperatures for the first and second polymerization were 123 °C and 132 °C, respectively, and that DCP was adopted as the polymerization initiator for the second polymerization, to obtain styrene-modified  
25 polyethylene-based resin particles, pre-expanded resin

particles and an expanded molded article thereof.

The gel fraction in the resin particles thus obtained was 1.8 wt%. The polystyrene content in the gel component was 24.4 wt% and the powder content in the polymerized 5 slurry was 0.6 wt%. The molecular weight of the polystyrene resin component was about 220,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a density of 33 kg/m<sup>3</sup>, a compressive strength of 40 N/cm<sup>2</sup>, and 10 falling ball impact value of 80 cm. The dimensional change rate under heat was 0.7%.

#### Comparative Example 8

40 kg of pure water, 200 g of magnesium pyrophosphate as a dispersant, and 20 g of sodium 15 dodecylbenzenesulfonate were introduced in an autoclave having an internal volume of 100 liter to prepare an aqueous medium. 8.0 kg of the polyethylene-based resin particles obtained in Example 1 was suspended in the medium and stirred at 150 rpm.

20 Into the autoclave, a mixed solution containing 32.0 kg of a styrene monomer (400 parts by weight relative to 100 parts by weight of polyethylene) and 96 g of TBPB (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60 minutes to 25 impregnate the styrene monomer into the polyethylene-based

resin particles. Then, the temperature was raised to 121 °C and polymerization was carried out for 5 hours. Subsequently, by raising to 140 °C and maintained for 2 hours, the remaining monomer was forcibly polymerized to reduce its  
5 amount, and then the autoclave was cooled to obtain styrene-modified polyethylene-based resin particles.

The gel fraction measured was 1.7 wt%. The polystyrene content in the gel component was 20.6 wt% and the powder content in the polymerized slurry was 1.8 wt%.  
10 The molecular weight of the polystyrene resin component was about 320,000.

Since the polymerized slurry contained a large amount of polymer powder and the powder impairs the fusibility of the expandable particles, fine pre-expanded resin particles and an  
15 expanded molded article could not be obtained.

#### Comparative Example 9

The same polymerization procedure as in Example 11 was repeated except that the respective amount of the polymerization initiator for the first and second polymerization  
20 was 0.3 parts by weight and that the mixed solution for the second polymerization was added after the conversion ratio of polymerization reached to 75%, to obtain styrene-modified polyethylene-based resin particles, pre-expanded resin particles and an expanded molded article thereof.

25 The gel fraction measured was 7.2 wt%. The

polystyrene content in the gel component was 22.2 wt%.

Since the excess styrene monomer was polymerized alone or on the surface of the polyethylene-based resin particles, the amount of the polymer powder generated was extremely large 5 such that the powder content in the polymerized slurry was 1.9 wt%. The molecular weight of the polystyrene resin component was about 320,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had a 10 density of 33 kg/m<sup>3</sup> and a compressive strength of 45 N/cm<sup>2</sup>. Since a large amount of polymer powder of polystyrene was generated and thereby fusibility of the expanded particles decreased, the falling ball impact value was as low as 40 cm. The dimensional change rate under heat was 0.4%.

15 A ratio between materials and polymerization conditions of Examples 1 to 13 and Comparative examples 1 to 9 are shown in Table 1. The gel fraction, polystyrene content, powder content, molecular weight of the polystyrene resin component, compressive strength, falling ball impact value and 20 dimensional change rate under heat are together shown in Table 2.

Table 1

		PE/PS (1 <sup>st</sup> & 2 <sup>nd</sup> )	Conversion Ratio of Polymeri- zation (%)	Polymeri- zation Temp. (1 <sup>st</sup> /2 <sup>nd</sup> ) (°C)	Polymeri- zation Initiator (1 <sup>st</sup> /2 <sup>nd</sup> )	Amount of Initiator (1 <sup>st</sup> /2 <sup>nd</sup> ) (wt %)
EXAMPLES	1	100/400 (200+200)	85	119/119	TPOEHC/TBPB	0.3/0.3
	2	100/400 (200+200)	85	121/121	TPOEHC/TBPB	0.3/0.3
	3	100/400 (200+200)	85	122/122	TPOEHC/TBPB	0.3/0.3
	4	100/400 (200+200)	85	123/123	TPOEHC/TBPB	0.3/0.3
	5	100/400 (200+200)	85	125/125	TPOEHC/TBPB	0.3/0.3
	6	100/800 (300+500)	85	122/122	TBPOEHC/TBPB	0.3/0.3
	7	100/400 (100+300)	85	119/121	TBPB/TBPB	0.3/0.3
	8	100/400 (100+300)	85	126/121	DCP/TBPB	0.3/0.3
	9	100/400 (100+300)	85	123/112	TBPB/TBPOTMH	0.3/0.3
	10	100/400 (100+300)	85	123/130	TBPB/DCP	0.3/0.3
	11	100/400 (100+300)	90	120/120	TBPB/TBPB	0.6/0.6
	12	100/400 (100+300)	95	120/120	TBPB/TBPB	0.3/0.3
	13	100/400 (100+300)	85	120/120	TBPB/TBPB	0.24/0.24
COMP. EXAMPLES	1	100/400 (200+200)	85	117/117	TPOEHC/TBPB	0.3/0.3
	2	100/400 (200+200)	85	130/130	DCP/DCP	0.3/0.3
	3	100/400 (200+200)	60	119/119	TPOEHC/TBPB	0.3/0.3
	4	100/400 (100+300)	85	117/121	TBPB/TBPB	0.3/0.3
	5	100/400 (100+300)	85	128/121	DCP/TBPB	0.3/0.3
	6	100/400 (100+300)	85	123/110	TBPB/TBPOTMH	0.3/0.3
	7	100/400 (100+300)	85	123/132	TBPB/DCP	0.3/0.3
	8	100/400	—	121	TBPB	0.3
	9	100/400 (200+200)	75	120/120	TBPB/TBPB	0.3/0.3

Table 2

	Gel Fraction (wt%)	PS Content (wt%)	Powder Content (wt%)	M. W. Ca. ( $\times 10^4$ )	Compressive Strength (N/cm <sup>2</sup> )	Falling Ball Impact Value (cm <sup>2</sup> )	Dimensional Change Rate under Heat (%)
1	7.2	22.2	0.7	32	40	85	0.4
2	26.5	21.9	0.8	31	42	95	0.3
3	33.5	20.9	0.7	30	44	95	0.2
4	20.8	22.1	0.6	29	42	90	0.3
5	5.8	34.5	0.5	28	40	85	0.4
6	38.5	21.3	0.8	30	48	85	0.2
7	7.2	25.0	0.5	30	43	85	0.4
8	3.5	22.8	0.5	30	42	85	0.4
9	3.2	24.4	0.5	34	43	85	0.3
10	3.8	24.2	0.6	24	43	85	0.4
11	19.6	25.0	0.7	26	40	90	0.4
12	18	23.3	0.3	32	46	95	0.3
13	17.5	24.6	0.5	32	46	95	0.2
1	0.3	26.6	0.5	33	36	80	0.8
2	0.8	25.0	0.8	24	38	80	0.7
3	5.6	21.4	1.6	32	38	60	0.8
4	1.6	25.0	0.5	30	38	80	0.7
5	1.8	25.0	0.6	30	40	80	0.7
6	2.6	25.0	0.5	36	37	50	0.4
7	1.8	24.4	0.6	22	40	80	0.7
8	1.7	20.6	1.8	32	—	—	—
9	7.2	22.2	1.9	32	45	40	0.4

Example 14

Polyethylene-based resin particles were obtained in the same manner as in Example 1 except that linear low-density polyethylene having a different melting point from 5 that used in Example 1 (ethylene-butene copolymer: melt index of 0.7 g/10 min, density of 0.922 g/ml, melting point of 121 °C) was used.

40 kg of pure water, 200 g of magnesium pyrophosphate as a dispersant, and 20 g of sodium 10 dodecylbenzenesulfonate were introduced in an autoclave having an internal volume of 100 liter to prepare an aqueous medium. 8.0 kg of the polyethylene-based resin particles was suspended in the medium and stirred at 150 rpm.

Into the autoclave, a mixed solution containing 8.0 kg 15 of a styrene monomer (100 parts by weight relative to 100 parts by weight of polyethylene) and 24.0 g of TBPB (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60 minutes to impregnate the styrene monomer into the 20 polyethylene-based resin particles. Then, the temperature was raised to 118 °C and polymerization was carried out for 3 hours.

After the conversion ratio of polymerization of the styrene monomer reached to 90%, a mixed solution containing

24.0 kg of a styrene monomer (300 parts by weight relative to 100 parts by weight of polyethylene) and 72.0 g of TBPB (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added at 118 °C over a period of 4 hours to 5 perform polymerization while impregnating the styrene monomer into the inside of polyethylene. Then, by raising to 140 °C and maintained for 2 hours, the remaining monomer was forcibly polymerized to reduce its amount, and then the autoclave was cooled to obtain styrene-modified 10 polyethylene-based resin particles. Pre-expanded resin particles and an expanded molded article were subsequently obtained in the same manner as in Example 1.

The gel fraction in the resin particles thus obtained was 29.8 wt%. The polystyrene content in the gel component 15 was 24.2 wt% and the powder content in the polymerized slurry was 0.5 wt%. The molecular weight of the polystyrene resin component was about 320,000.

The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had 20 excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 43 N/cm<sup>2</sup>, and falling ball impact value as high as 90 cm. The dimensional change rate under heat was 0.2%.

The ratio between materials, polymerization conditions, powder content, gel fraction, polystyrene content, molecular 25 weight of the polystyrene resin component, falling ball impact

value, compressive strength and dimensional change rate under heat of Example 14 are together shown in Table 3.

Table 3

PE/PS(1 <sup>st</sup> and 2 <sup>nd</sup> )	100/400(100/300)
Polymerization Temperature (1 <sup>st</sup> /2 <sup>nd</sup> ) (°C)	118/118
Conversion ratio of polymerization(%)	90
Polymerization Initiator(1 <sup>st</sup> /2 <sup>nd</sup> )	TBPB/TBPB
Amount of Initiator (1 <sup>st</sup> /2 <sup>nd</sup> ) (wt%)	0.3/0.3
Gel Fraction(%)	29.8
PS Content(wt%)	24.2
Powder Content(wt%)	0.5
M. W. ( $\times 10^4$ )	About 32
Falling Ball Impact Value(cm <sup>2</sup> )	90
Compressive Strength(N/cm <sup>2</sup> )	43
Dimensional Change Rate under Heat(%)	0.2

5 As seen in Table 3, it is understood that an expanded molded article having excellent impact resistance, stiffness, and heat resistance can be provided even with the polyethylene-based resin having the different melting point.

#### Example 15

10 40 kg of pure water, 200 g of magnesium pyrophosphate as a dispersant, and 20 g of sodium dodecylbenzenesulfonate were introduced in an autoclave having an internal volume of 100 liter to prepare an aqueous medium. 8.0 kg of the polyethylene-based resin particles  
15 obtained in Example 1 was suspended in the medium and stirred at 150 rpm.

Into the autoclave, a mixed solution containing 3.2 kg of a styrene monomer (400 parts by weight relative to 100 parts by weight of polyethylene) and 9.6 g of DCP (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added and allowed to stand at 60 °C for 60 minutes to impregnate the styrene monomer into the polyethylene-based resin particles. Then, the temperature was raised to 126 °C and polymerization was carried out for 3 hours.

After the conversion ratio of polymerization of the styrene monomer reached to 90%, a mixed solution containing 28.6 kg of a styrene monomer (358 parts by weight relative to 100 parts by weight of polyethylene), 0.2 kg of α -methyl styrene (2 parts by weight relative to 100 parts by weight of polyethylene) and 86.4 g of TBPB (0.3 parts by weight relative to 100 parts by weight of the styrene monomer) was added at 122 °C over a period of 5 hours to perform polymerization while impregnating styrene into the inside of polyethylene. Then, by raising to 140 °C and maintained for 2 hours, the remaining monomer was forcibly polymerized to reduce its amount, and then the autoclave was cooled to obtain styrene-modified polyethylene-based resin particles.

Pre-expanded resin particles and an expanded molded article were subsequently obtained in the same manner as in Example 1.

The gel fraction in the resin particles thus obtained

was 30.6 wt%. The polystyrene content in the gel component was 25.0 wt% and the powder content in the polymerized slurry was 0.8 wt%. The molecular weight of the polystyrene resin component was about 300,000.

5 The pre-expanded resin particles had a bulk density of 33 kg/m<sup>3</sup>. The expanded molded article thus obtained had excellent strength, showing a density of 33 kg/m<sup>3</sup>, compressive strength of 42 N/cm<sup>2</sup>, and falling ball impact value as high as 90 cm. The dimensional change rate under heat was 0.2%.

10 The ratio between materials, polymerization conditions, powder content, gel fraction, polystyrene content, molecular weight of the polystyrene resin component, falling ball impact value, compressive strength and dimensional change rate under heat of Example 15 are together shown in Table 4.

Table 4

PE/PS(1 <sup>st</sup> and 2 <sup>nd</sup> )	100/400(40/360)
Polymerization temperature(1 <sup>st</sup> /2 <sup>nd</sup> ) (°C)	126/122
Conversion ratio of polymerization(%)	90
Polymerization Initiator(1 <sup>st</sup> /2 <sup>nd</sup> )	DCP/TBPB
Amount of Initiator(1 <sup>st</sup> /2 <sup>nd</sup> ) (wt%)	0.3/0.3
Gel Fraction(%)	30.6
PS Content(wt%)	25.0
Powder Content(wt%)	0.8
M. W. (×10 <sup>4</sup> )	約 30
Falling Ball Impact Value(cm*)	90
Compressive Strength(N/cm <sup>2</sup> )	42
Dimensional Change Rate under Heat(%)	0.2

As seen in Table 4, it is understood that an expanded molded article having excellent impact resistance, stiffness, and heat resistance can be provided even with a mixture of two different styrene monomers.

5

As described hereinbefore, by controlling selection of the polymerization initiator and the polymerization temperature at impregnation and polymerization of the styrene monomer into the polyethylene-based resin particles for 10 polymerization, the expandable particles of the styrene-modified linear low-density polyethylene-based resin which control the gel fraction and which satisfy physical properties such as impact resistance, stiffness, and heat resistance can be provided.

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